

The Potential of Temporary Immersion Bioreactors (TIBs) in Meeting Crop Production Demand in Nigeria

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Abstract

Micropropagation, popularly known for large-scale clonal propagation, is the first major and widely accepted practical application of plant biotechnology. The commercial utility of conventional micropropagation of important crop species is limited as a result of the large numbers needed annually to start up new farms in addition to high production costs. These result primarily from high labour cost, low multiplication rate or long duration of multiplication before plantlets are taken to the field, and poor survival rates resulting from contamination risks and during acclimatization. All of these constitute a major setback in the use of Micropropagation for scaling up of the several economic species for commercialization. Temporary Immersion Bioreactor system (TIBs) is a relatively recent micropropagation procedure that employs the use of automated gadgets to control rapid multiplication of plant cultures under adequate conditions. TIBs provide a more precise control of the adequate conditions (gaseous exchange, illumination etc.) required by plants for growth, development and survival than the conventional culture vessels. This bioreactor system incorporates a number of features specifically designed to simplify its operation and reduce production costs. The set-up consists of two vessels, one for the plantlets and the other one for the liquid culture media coupled together through a perforated rubber tubing that permits the flow of the liquid media from one vessel to the other. TIBs consist of three main phases: Multiplication, Elongation and Rooting phase. Plantlets propagated in TIBs have better performance than those propagated by conventional methods of micropropagation. This is as a result of a better handling of the in vitro atmosphere and the nutrition. TIBs provide a rapid and efficient plant propagation system for many agricultural and forestry species, utilizing liquid media to avoid intensive manual handling. In addition to diminishing production costs regarding labour force, Temporary Immersion Bioreactors save energy, augment micropropagation productivity and efficiency.

Keywords: Temporary Immersion Bioreactors, Scale-up, Micropropagation



1. Introduction

New contributions to *in vitro* techniques for plant propagation in the last decade has simplified micropropagation technology and at the same time open up new avenues of challenges. It took scientists and researchers a number of steps and lots of effort to arrive at the various micropropagation protocols and techniques, routinely applied today in most laboratories. Research have over time, risen from a myriad of challenges to what appears to be less challenging but the mystery behind this is at every new level, there is a new encounter that limits the adequate achievement of the new task.

Plant regeneration in vitro is dependent on the manipulation of the inorganic and organic constituents in the medium, as well as the type of explant and the species. In most plant species, successful regeneration from the callus or directly from the explants takes place after a series of subcultures on various media, in a sequence which is often specific to the species, variety, or the newly introduced genotype. The determining factors are the combination of the concentration in relation to medium volume and the composition of growth promoting and retarding regulators in the medium, the physiological status and competence of the cells and their capability for morphogenetic expression (Christianson, 1985; 1987).

In micropropagation, all plant somatic cells once isolated and cultured in vitro are capable of expressing totipotency. Regeneration is potentiated through two morphogenic pathways:

Organogenesis which is the formation of unipolar organs and Somatic embryogenesis which is the production of somatic embryos with a root and a shoot meristem (Steward et al., 1970; Ammirato et al., 1985). After many decades of research and development, conventional micropropagation techniques are still not always reliable. The commercial utility of conventional micropropagation of most important crop species is limited and scaling-up is not always easy. Nevertheless, their application in horticulture, agriculture, and forestry is currently still expanding worldwide. In order to overcome the problems of conventional micropropagation, protocols have been proposed using bioreactors and liquid medium (Tautorus et al., 1995; Weathers et al., 1989; Takayama and Akita, 1994; Teisson and Alvard, 1995). Automation, using a bioreactor, is one of the most effective ways to reduce the costs of micropropagation (Aitken-Christie et al., 1995; Levin et al., 1998). In temporary immersion bioreactors, the cultures are immersed in the medium, for a preset duration at specified intervals. A typical design, utilizes two vessels (plastic or glass) of which one holds the liquid medium and the other the cultures (Adelberg and Simpson, 2002). Temporary immersion bioreactors are simple and cost effective to run. Consequently, a number of commercial micropropagation laboratories have begun to integrate these systems into their production procedures. Temporary Immersion Bioreactors (TIBs) generally reduces some problems usually encountered in permanent liquid cultures such as hyperhydricity, poor quality of propagules, and necessity of transplanting on a solid medium in the elongation and/or rooting stage. In comparison with conventional micropropagation on semisolid medium, the TIB provides a superior mass balance. Indeed in the latter comparison the proliferation rate is higher, labor efficiency is improved and, as a consequence, the cost is reduced (Teisson and Alvard, 1995; Escalona et al., 1999; Etienne et al., 2006). Recently, the effect of environmental



conditions, such as nutrient supply and composition of the internal atmosphere in the culture vessel, on the physiology of some species in the recipient for automated temporary immersion system (RITA) has been reported (Martre *et al.*, 2001; Escalona *et al.*, 2003). This definition of physiological requirements of explants and eco-physiological characterization of the bioreactor environment has contributed immensely to facilitate an increase in plant quality. This paper reviews the potential benefits and importance of TIBs; and how it can be applied as a tool for scaling up economically important species to enhance food security in Nigeria.



Figure 1. Temporary immersion bioreactor set up at NACGRAB.

1.1 Importance of TIBs technology to national development.

Modern biotechnology has put the micropropagation industry on the verge of exciting new breakthroughs. It offers improvements in virtually every area of crop production and utilization, with potential benefits to agriculture, the food industry, consumers and the environment. As the world's population continues to grow, it is anticipated that there could be many mouths to feed in the next few decades. The advances made possible through micropropagation (TIBs) will be essential to meet global food needs by increasing the yield, quality and quantity of crops available to farmers. TIBs offer further benefits in form of non-food crops. Through mass propagation of specific economic species, it will be possible to arrest desertification, soil erosion in affected areas and also increase industrial crop production as renewable sources of medicines, industrial chemicals, fuels etc. They offer potential benefits to the commercial farmers, industries, public, research scientists and students. The potential benefits of TIBs are summarized below.

• Mass propagation of agronomic food crops (food security). All year round production and supply of planting materials to farmers.



- Scaling up of the production of specific crops for industrial use (A step towards commercialization) e.g pineapple juice.
- Mass propagation of economic tree species (e.g *Eucalyptus spp., Adzadiracta indica* Neem, *Accacia senegalensis* Gum Arabic) for addressing environmental problems like desertification and erosion.
- Job creation.
- Inspire collaborations among institutions on specific projects.

1.2 Apparatus for setting up TIBs.

TIBs technology requires advance automation procedure and as such setting up will require a number of equipment with unique specification and functions, proficiency in operation techniques and expertise. The knowledge about the interactions between plant physiology and the physical parameters in the bioreactor design is very crucial as lack of this knowledge will affect the efficient use and sustainability of the technology. At the National Centre for Genetic Resources and Biotechnology (NACGRAB), Ibadan, Nigeria, the following components have been acquired and utilized in setting up TIBs.

1.2.1 Oil Free Compressor

The oil free air compressor uses a motorized rotor to compress air. The oil free compressor is used in this system because entrained oil carry-over will interfere with the proper functioning of the Temporary Immersion System (TIS), as it could be a likely source of contamination.

1.2.2 PVC tubes

Tubes of varying sizes are used in this system as the channel for the transfer of compressed air between the compressor and the bioreactor vessels. The larger (0.5mm) diameter tubing are to connect from the solenoid valve and terminate at the 'T' connectors, the medium sized (0.35mm) pvc/silicon tubing to connect from the 'T' connector to one end of the micropore filter. The smaller PVC/silicon tubing are connected from the filter to the bioreactor vessel and also interconnects the bioreactor vessels. The need to maintain sterility at this stage mandates the use of autoclaveable tubings. This is to allow repetitive use of tubing.

1.2.3 'T' connectors

At the initial stage of this project the use of copper 'T' connectors was used but there was a need to extend the ducts by welding to make it suitable. Later in the life of the project, the use of ready-made brass 'T' connectors that fitted suitably into the Temporary Immersion System (TIS) was employed. Some of the factors to consider in the choice of the material for a 'T' connector are its ability to withstand high pressure and resistance to corrosion (rusting).

1.2.4 Hydrophobic micro pore filters (membrane)

These are sterilizing grade filters with 0.22μ m permeability that provides a sterility assurance, high flow rate and throughput (fig3). It is used in the system for filtration of the air coming from the compressor; this membrane serves as a sieve to eliminate contaminants and



microorganisms, as well addressing the need to remove hydrocarbons ingested from the ambient.

1.2.5 Clips

In instances where deemed necessary clips are used to fasten the ends of the tubing. This serves in preventing disconnection during flow.

1.2.6 Solenoid valve

A solenoid valve is an electromechanical device which consists of two main parts as the name implies a solenoid and a valve. The solenoid converts electrical energy to mechanical energy, which in turn opens and closes the valve. The solenoid valve is controlled by an electric current, the solenoid creates a controlled magnetic field when electrical current passes through it causing the valve to open or close. It is mainly used to control air flow in the TIS.

1.2.7 Programmable timer

An electronic timer is used to control the sequence of an event or process. The programmable timer is used in TIS to control the flow of electric current into the solenoid valves.

1.2.8 Barometer

This is used to control the air pressure within the tank and regulate the outlet pressure.

1.2.9 Shelves

This is the mainframe on which the TIS is built. It comprises of the stand and the required number of layers. The layers are either of a perforated material or transparent sheets.

1.2.10 Bioreactor vessels

These are bottles usually made of glass or plastic having a volume between 0.5 to 5.0 liters. It is provided with a securing cover that can be opened for the replacement of media and removal of plants as may be required. Two holes are perforated on the cover to serve as inlet/outlet to air and the media tubing.

1.2.11 Electrical accessories

This will include electrical fittings, cables and insulators mainly for illumination. Lighting is very important in TIS as it permits the occurrence of some metabolic activities such as photosynthesis.

2. Operational Mechanism

This system requires steady power supply for its successful operation. The air compressor is powered until the 25 liters capacity tank (as applied in this case study) is filled with air at a pressure of 8bar which could be regulated according to user's requirement. The outlet pressure is set to 1.5bar taking into consideration important factors such as the air travelling distance, size and number of vessels in the system. The air is let into the system at required pressure and its flow is controlled by the solenoid valves. A total of four solenoid valves (1,2, 3 & 4) are



needed to put the system in a functional state, the valves operate in pairs of inlet and outlet each with 1 & 4 being the inlet valves and 2 & 3 being the outlet valves respectively. For optimum operation valve 1 pairs with valve 3 (inlet/outlet) and valve 4 pairs with valve 2. For the purpose of this study, four feeding cycles have been adopted, lasting between the hours of 9:00am and 6:00pm at 3 hours interval. The operational cycles can be varied dependent on the availability of power supply and plant nutrient requirements. The air is pneumatically driven through the connecting pipes via the solenoid valve allowing the flow of air into the system. This is achieved by the use of programmeable timers which permits the flow of electric current at the designated periods. With this, pressurized air through the hydrophobic micropore filters is introduced into the bioreactor vessels, thus automating the system.



Figure 2. Schematic illustration describing the operation process of TIS following the given explanation

Source: Escalona (1999).

The system utilizes two culture vessels one containing the shoots and the second the liquid culture medium. Valve 3 (V3) is opened 10 secs prior to the opening of valve 1 (V1) to discharge excessive pressure in the system. This is to avoid damage or disconnection of connecting tubes and vessels resulting from high pressure. Pressurized air enters into bioreactor vessel A through the autoclaveable tube 1 at the opening of valve 1. The air pressure in the vessel displaces the liquid medium through tube 2. The pumping duration of the medium is also dependent on the quantity of medium in the bottle. It is important to note that excessive bubbling during the feeding cycle has been reported by Ziv (2000) to have a deterrent effect on plants in TIS. For use in this study a pumping duration of 2 minutes is employed during transfer of 250ml of medium from vessel A to vessel B. The period of immersion could also vary, based



on specific plant requirements. The name of the system is basically derived from this process where plants are immersed temporarily, and again the immersion period depends on individual plant species under study.

After completion of the desired immersion period, a reverse process similar to the process explained above takes places again, this time around returning media to vessel A. Valve 2 (outlet) is opened and valve 4 is also opened 10secs later. This is accompanied by the inflow of pressurized air via tube 3, displacing the medium in vessel B. The medium is withdrawn through tube 2 into vessel A. This cycle is continually repeated at the prescribed intervals (3 hours in this study) to ensure adequate nutrient uptake and nourishment of plants in TIS.



Figure 3: Accessories used in TIBs. Hydrophobic micropore filter of 0.22ul; Transparent vessel with cover of two holes and Connect tubing

Source: Aragon et al., 2009.

3. Stages Involved in TIBs

The process of plant micro-propagation aims to produce clones (true copies of a plant in large numbers). Four major stages are recommended for effective mass propagation of plant cultures using temporary immersion systems are subsequently explained.

3.1.1 Establishment of the mother explants on agar gel medium.

The establishment of truly aseptic cultures usually involves the following sequential steps:

Step I- Pre-propagation step or selection and pre-treatment of suitable plants.

This is the selection, screening and treatment of plants collected from the field before taking into the laboratory environment. The health status of the donor mother plant and of the plants multiplied from it are among the most critical factors, which determine the success of tissue culture operation. Hence, indexing of the mother plants for freedom from viral, bacterial, and fungal diseases is a normal procedure before undertaking propagation in large-scale plant propagation through tissue culture (Schmidt et al., 2002). This step is crucial as it tends to reduce the microbial load present at the time of collection and which may hinder or interfere

with the in vitro processes. The plants upon treatment are observed in the green house for a short period of time before transfer into the laboratory. Pre-propagation step (also called stage 1) requires proper maintenance of the mother plants in the greenhouse under disease- and insect-free conditions with minimal dust. Clean enclosed areas, glasshouses, plastic tunnels, and net-covered tunnels, provide high quality explant source with minimal infection. Collection of plant material for clonal propagation should be done after appropriate pretreatment of the mother plants with fungicides and pesticides to minimize contamination in the in vitro cultures. This improves growth and multiplication rates of in vitro cultures. The control of contamination begins with the pretreatment of the donor plants. They may be prescreened for diseases, isolated and treated to reduce contamination (Martre, et al., 2001).

Step II - Initiation of explants - surface sterilization, establishment of mother explants.

This involves the sequential disinfection of the mother plant under aseptic conditions, culture initiation and establishment on a suitable growth media. The process requires excision of tiny plant pieces and their surface sterilization with chemicals such as sodium hypochlorite, ethyl alcohol and repeated washing with sterile distilled water before and after treatment with chemicals. The growth media is prepared in the preparatory room while the rest of the process is carried out under the laminar flow hood. The initiated cultures are then transferred to the growth room under controlled conditions of temperature, illumination and humidity for incubation. Initiation of explants is the very first step in micropropagation. A good clean explant, once established in an aseptic condition should be regarded as a critical step in micropropagation.

Step III - Subculture of explants on agar gelled media for multiplication and proliferation.

This involves the subculture of established explants on agar gelled media with a specific auxin/cytokinins combination to induce proliferation. In this step, explants are cultured on the appropriate media for multiplication of shoots. The primary goal is to achieve propagation without losing the genetic stability. Repeated culture of axillary and adventitious shoots, cutting of nodes, somatic embryos and other organs from Stage II lead to multiplication of propagules in large numbers. The propagules produced at this stage can be further used for multiplication by their repeated culture.

3.1.2 Zero shelving of plants to liquid medium.

Sometimes it is necessary to subculture the in vitro derived shoots onto different media for elongation and rooting for ex vitro transfer. However, if cultures must be mass propagated in Temporary Immersion System, they must be allowed to pass through the zero phase upon establishment and when they have gained a proliferation capacity/potential on the agar gelled multiplication media. This involves the gradual reduction of agar concentration in the nutrient medium from semi solid to liquid medium. This is usually done in order to prepare the explants for proper adaptation, survival and desired in vitro response in the next phase which utilizes only liquid medium. Zero shelving also gives room for proper check of microbial contamination that may be present in the culture and selection of healthy propagules prior to



transferring into the temporary immersion systems. If contamination is noticed, the plantlets are retrieved and rescued. In situation whereby the contaminant persists, cultures are discarded. All other growth conditions are the same as mentioned earlier.

3.1.3 Cultivation in Temporary Immersion Systems.

This Phase refers to Plant cell and tissue development in the Temporary immersion bioreactors. It utilizes the advantages of liquid medium coupled with automated control of culture conditions to rapidly multiply explants thereby increasing exponentially the multiplication coefficient of the explants. The stage involves 3 major phases (Figure 4). They are:

- Multiplication phase
- Elongation phase
- Rooting and harvest

In vitro response of plantlets in each of the 3 phases of TIBs is highly dependent on certain factors including hormonal combination, duration of each feeding cycle and the overall timing/duration to which it is subjected to. eg. higher cytokinins (BAP) concentration to auxins in the multiplication media, Gibberillic acid (GA3) for elongation and auxins (IAA, NAA and IBA) for rooting. The timing to achieve goal at each phase varies depending on the individual species ability to respond to each phase accordingly. The common feature to all the phases is the use of liquid media (void of agar) to aid nutrient uptake and automation. Transfer of plantlets from one step to the next is carried out aseptically under the laminar flow hood. If the proliferated material consists of bud-like structures (e.g. orchids) or clumps of shoots (banana, pineapple), they should be separated after rooting and not before as this usually cause tissue wounding and stimulate the exudation of phenolic compound which interferes with the physicochemical factors that trigger root formation. This leads to malformed plants or plants with no roots. In this way, multiplied plantlets are elongated, rooted to produce complete plants and harvested. Harvest is carried out by an initial disinfection of the mouth of culture bottle with 1% Sodium hypochlorite. Bottle is opened and plantlets carefully collected.



Figure 4: Multiplication (1st picture showing proliferation in clusters); Elongation (2nd picture showing stem growth elongation) and Rooting (3rd picture clearly showing a developed root system) of pineapple in TIBs at NACGRAB

3.1.4 Acclimatization and Ex vitro transfer.

This is the final stage of the tissue culture operation including the use of bioreactor after which the micro propagated plantlets are ready for transfer to the greenhouse. Steps are taken to grow individual plantlets capable of carrying out photosynthesis. Collected plantlets are sorted and prepared for acclimatization based on their sizes and rooting capacity. In vitro micro propagated plants are weaned and hardened. The hardening of the bioreactor propagated plantlets is done gradually from high to low humidity and from low light intensity to high intensity conditions. Rooted plants are washed with tap water and acclimatized ex vitro on a medium composed of Coconut fibre, Top Soil and Stone dust mixed in the ratio 7:2:1 which can be left in shade for 3 to 6 days where diffused natural light conditions them to the new environment. The plants are then transferred to an appropriate substrate (sand, peat, compost, etc.), and gradually hardened. Low-cost options include the use of plastic domes or bags, which reduces the natural light intensity and maintains high relative humidity during the hardening process. If the plants are still joined together after rooting, these should be planted as bunches in the soil and separated after 6 to 8 weeks of growth.



Figure 5: Potted and acclimatized TIBs base plants in the screen house at NACGRAB

These stages are universally applicable in large-scale multiplication of plants. The individual plant species, varieties and clones require specific modification of the growth media, weaning and hardening conditions. A rule of the thumb is to propagate plants under conditions as natural or similar to those in which the plants will be ultimately grown ex-vitro. Micropropagated plants must be subjected to an adequate duration of time required for their proper hardening.

3.2 Growth Conditions in Temporary Immersion Bioreactors

Conditions for growth and maintenance of in vitro cultures in Temporary Immersion Bioreactors include:

- 1. Natural and Artificial Photoperiod for cultures which should be 16 hours light per day.
- 2. Incubation Temperature (20 ± 2 °C).
- 3. The culture media which should have a pH of 5.7 ± 1 (that is to say 5.6-5.8 range).



- 4. The culture media volume (100 250ml for 500ml and 300 400 for 11itrer capacity vessel).
- 5. Observation of 8 immersions per day with 3 hours interval. This condition is dependent on the plant species.
- 6. The duration of immersion of cultures in the media should range between 3-5 minutes depending on the plant species.
- 7. Duration of the *in vitro* process:
 - ➤ Multiplication phase: 4 -6weeks depending on the species.
 - Elongation phase: 2 3 weeks and is species dependent.
 - \triangleright Rooting phase: 3-4 weeks.

Plant	Propagule unit produced	Reference	
Amaryllis hippeastrum	Buds, bulblets.	Takayama and Akita, (1998)	
Apium graveolens	Somatic embryos	Nade et al., 1990.	
Ananas comosus.	Shoot clusters		
Apium graveolens.	Somatic embryos.	Nade et al., 1990	
Araceae species	Plants Takayama and Akita, 1998.		
Acanthopanax koreanum.	Somatic embryos. Son et al., 1999b		
Artemisa annua	Plants. Park et al., 1989.		
Asparagus officinalis.		Fakayama, 1991.	
Begonia	Multiple shoots	Takayama and Misawa, 1981	
Brodiaea species.	Bud clusters, cormsIlan et al., 1995.		
Colocasia species.		Takayama, 1991.	
Coffea arabica.	Shoot clusters, plants.	Teisson and Alard, 1995.	
Cyclamen persicum	Somatic embryos	Hvoslef-Eide and Munstar, 1998	
Daucus carota	Somatic embryos	atic embryos Jay et al., 1992.	
Dianthus caryophyllus	Shoots, plants. Chatterjee et al., 1997.		
Digitalis lanata.	Somatic embryos. Greidziak et al., 1990.		
Eschcholltzia californica.	Somatic embryos. Archambault et al., 1994		
Euphorbia puleherrima	Somatic embryos.	Preil, 1991.	
Fragaria ananasa	Shoots, plants.	Takayama and Akita, 1998.	
Gentiana species.	Plants.	Hosokawa et al., 1998.	
Gladiolus grandiflorum	Bud clusters, corms.	Ziv et al., 1994; Teisson and alvard, 1995.	
Gloximia	Shoots	Takayama, 1991	
Hevea brasiliensis	Buds, plants Alvard et al., 1993; Teisson and Alvard, 19		
Hyacinthus orientalis.	Bulblets, plants.	Takayama and Akita, 1998.	

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Lilium species	Plants, bulblets	Takayama 1991.	
Medicago sativa	Somatic embryos.	Stuart et al., 1987.	
Musa species	Buds, plants	Alvard et al., 1993.	
Nephrolepts exaltata	Buds, plants	Levin et al., 1997; Ziv et al., 1998	
Nerine sarniensis.	Bulblets, somatic embryos.	Lilien-Kipnis et al., 1994; Ziv et al., 1994	
Ornithogalum dubium.	Shoots, bulblets, plans.	Ziv and Lilien Kipnis, 1997.	
Populus tremula.	Bud cluster, shoots.	McCown et al., 1988.	
Picea species	Somatic embryos.	Tautorus et al., 1994; Attree et al., 1994.	
Pinellia ternate.	Shoots, corm.	Takayama et al., 1991.	
Phalaenopsis.	Protocorm.	Young et al., 2000.	
Solanum tuberosum.	Clusters, shoots.	Takayama and Akita, 1998; Ziv et al., 1998.	
Stevia rebaudiana	Shoots	Akita et al., 1994	

Source: Mehrotra, 2007.

Table 2: Effect of Temporary Immersion Bioreactor (TIBs) On Biological Yield

Crop	Variety	Conventional	Temporary
		micropropagation	immersion systems
Pineapple	Smooth cayenne	8.0	68.8
	MD2	5.8	26.8
Sugarcane	C91-301	3.7	34.1
	C1051-73	4.1	58.0
	C120-78	3.9	30.2
	C323-68	4.3	39.5
	Cp-5243	4.0	32.5
Taro	INIVIT	3.0	10.4
	Mexico 1	2.8	7.7
Banana	FHIA-18	3.8	7.4
	FHIA-01	3.4	10.4
	Grand Nane	4.0	16.6
Plantain	CEMSA 3/4	2.5	7.8
Eucalyptus	Urograndis	2.7	11.6
Syngonium	W. Butterfly	7.3	28.0
	Pixle	2.2	18.4
Philodendron	xanadu	2.0	8.8
Spathyphyllum	sensation	3.7	17.6

Source: Escalona, 2003.

3.3 Challenges

The use of liquid cultures in bioreactor for plant propagation imposes several problems such as leakage of endogenous growth factors, the need for an initial high concentration of the inoculum, lack of protocols and production procedures, increased hyperhydricity and malformation, foam development, shearing and oxidative stress, release of growth inhibiting www.macrothink.org/jbls

compounds by the cultures and contamination. Unfortunately culture contamination which is a major problem in conventional commercial micropropagation is even more acute in bioreactors (Leifert and Waites, 1998). In conventional micropropagation, discarding a small number of the contaminated vessels is an acceptable loss; in bioreactors, even a single contaminated unit is a huge loss. However, despite these difficulties, a number of commercial laboratories have developed effective procedures to control contamination in bioreactors. Highlighted below are some of the challenges (Leifert and Waites, 1990; Leifert and Woodward, 1998; Leifert, 2000).

3.3.1 Inadequate protocols and production procedures.

Plant cultures in bioreactor required defined protocol to enhance efficiency and optimization. Lack of protocol for maintenance of cultures in bioreactors affects the potential scale up of plants especially for commercialization (Espinosa et al., 2002) Regeneration and initial establishment of cultures is more often accomplished on agar gelled medium. For scaling up plant production using bioreactors, in vitro protocols that can accommodate the proliferation of plant cultures in liquid medium needs to be developed. Protocols for proliferation on semi solid media are not always efficient when used in bioreactors. However, as no one protocol is utilized for all species, it becomes quite difficult to achieve success at a goal. Development of protocol for scaling up cultures in bioreactors entails extensive research and development in all phases of TIBs (multiplication, elongation and rooting). It is possible to record success at one phase and not overcome the challenges at the next phase. For the efficient scaling up of cultures in temporary immersion bioreactors for commercialization, protocol for multiplication, elongation and rooting nust be developed.

3.3.2 Increased hyperhydricity and malformation.

The major disadvantage encountered when plants are cultured in liquid media is the problem of shoot malformation. Plants tend to accumulate excess of water in their tissue resulting to anomalous morphogenesis, a phenomenon known as Hyperhydricity. The plants that develop in liquid media are fragile, have a glassy appearance, with succulent leaves or shoots and a poor root system (Etienne, et al., 1997; Teisson, et al., 1995; Ziv, 1995). The leaves are the organs affected most severely in liquid cultures. They develop an unorganized mesophyll tissue that is made up mainly of spongy parenchyma tissue with large intercellular spaces (Etienne, et al. 2006), a deformed vascular tissue, and an abnormal epidermis. The epidermal tissue in hyperhydric leaves lacks a well developed cuticle and possesses malfunctioning guard cells which cannot respond to closure signals (Ziv et al. 1991; Ziv 1997; Ziv 2005). Hyperhydricity affects plant survival after transplanting and causes loss of the in vitro developed leaves, or even whole plants, which often wilt and die. The two major processes carried out by the leaves, photosynthesis and transpiration, are not fully functional in hyperhydric leaves and thus cause the poor performance of the transplanted plants ex vitro (Preece and Sutter 1991; Ziv, 1998., Ziv, 1995). In many plants propagated in vitro, the anomalous morphology and anatomical aberration often observed in plants result from deviation from the normal course of morphogenic events that are manifested in plants in vivo (Ammirato, 1985; Ziv, 2000).

The excessive accumulation of water in plant tissue (the most characteristic symptom of hyperhydricity) can also result in oxygen depletion in the cells, induce oxidative stress,

production of reactive oxygen species (ROS) and cause injury to the plant tissue. Several developmental processes in tissue cultured plants can be affected by ROS leading to recalcitrance and loss of morphogenetic competence (Etienne, 2006). ROS such as H2O2 and hydroxyl free-radicals react instantaneously with almost any substrates (Ziv, 2000). Attempts to control hyperhydric deformities have focused on better aeration and intermittent plant submergence in the medium, using temporary immersion bioreactors (Teisson, et al., 1996; Escalona, et al., 1999). Growth retardants have been used to reduce leaf expansion, thus minimizing shoot malformation. Some of the deformation, such as hyperhydric, malformed leaves and shoots, abnormal embryos, recurrent embryogenesis, and several other disorders (Ziv 1992, 1999, 2000), are apparently the result of interruption or faulty timing of the signals involved in the normal sequence of organizational events known to exist in vivo. These are problems that are manifested more severely in liquid medium and await further studies in order to understand and to help control plant morphogenic events in bioreactor cultures.

The following Suggestions have been known to reduce hyperhydricity problems in liquid media.

- Paper bridges or sponges (Escalona, *et al.*, 2003).
- Double layer adding liquid medium to established culture on agar (Escalona, 1999).
- Mist Bioreactors (Teisson, et al., 1995).
- Temporary Immersion (Alvard, *et al.*, 1993).
- A raft to support plants over stationary liquid (Hamilton et al., 1985).

3.3.3 Problems of foaming, shear and oxidative stress.

Growth and proliferation of the biomass in bioreactors depends on airflow supply for the aeration and mixing, and for the prevention of the plant biomass sedimentation. In many plants cultivated in bioreactors, continuous aeration, mixing, and circulation cause shearing damage, cell wall breakdown, and accumulation of cell debris, which is made up mainly of polysaccharides. Cell debris accumulation leads to the adhesion of cells and aggregates to the culture vessel walls which results in foaming and the development of a "crust" at the upper part of the bioreactor vessel. This layer prevents adequate liquid circulation and oxygen supply, causing additional cell debris formation and a demand for higher aeration rates that intensify the clogging problem (Scragg 1992). As the biomass increases and the cultures become viscous, higher rates of aeration are required to allow for oxygen supply and circulation. Several authors (Takayama, et al., 1991; Ziv, 1992; and Ziv 1998) have reported potential solutions to the problem of foaming and shear damage of tissues in bioreactors.

3.3.4 Release of growth inhibiting compounds by the cultures.

This is also known as the in vitro Phenolic browning or oxidation. The presence of phenolic compounds which cause death of explants has been another important problem of micropropagation especially in woody perennials (Ziv, 2005), in addition to various bacterial and fungal infection. Some of these exudates appear as a reaction to injury and/or infection. In

tissue culture they appear after tissue excision and are many times aggravated by growth media constituents (Seneviratne and Wijesekara, 1996). Tissue blackening occurs due to action of copper-containing oxidase enzymes: polyphenoloxidases like tyrosinases, which are released or synthesized in oxidative conditions after tissue wounding and they oxidize O-diphenols released due to cellular wounding to o-quinones (Gamborg, 2002). The onset of tissue browning has been found to be associated with changes in protein pattern, amino acid content, ethylene production and the occurrence of saccharose and accumulation of starch (Fowler, 2000). These changes eventually lead to growth inhibition or death of explants. Other types of phenolic exudates appear at the end of incubation period and are apparently products of dying cells (Seneviratne and Wijesekara, 1996). The phenolic exudation is aided by light and is autocatalytic.

A number of methodologies have been employed to overcome phenolic oxidation in in vitro techniques. Some of them as suggested by Pierik, 1987; are as follows:

- Addition of activated charcoal (0.2-3.0% w/v) to the medium.
- Addition of polymeric polyvinylpyrrolidone (PVP) or polyvinylpolypyrrolidone (PVPP) to the medium. These absorb phenols through hydrogen bonding.
- Additions of anti-oxidants or reducing agents like citric and ascorbic acids, thiourea glutathione and L-cysteine in the medium or before surface sterilization. These reduce the redox potential of explants and stop the oxidation reactions (Marks and Simpson, 1990).
- Addition of diethyl-dithiocarbonate (DIECA) (2g.l-1) in the rinses after surface sterilization and as droplets at the time of micro grafting.
- Addition of amino acids like glutamine, arginine and asparagine to the media.
- Reduction of salt concentration in the growth media. Others may include:
- Frequent subcultures onto fresh media.
- Use of liquid medium for easier and quicker dilution of toxic products.
- Reduction of wounded tissues to decrease exudation.
- Soaking of explants in water before culturing to reduce browning.
- Incubation of fresh cultures in darkness for the first few days of culture.

Most of the suggested above have provided solution to phenolic oxidation in micropropagation and are widely employed in most laboratory across the globe.

3.3.5 Microbial contamination

Micropropagation techniques are extensively used for mass production of elite plants as well as to study the basic aspects of primary and secondary metabolism, morphogenesis and genetic engineering etc. But even after three decades of research and development in plant tissue culture, microbial contamination by yeasts, fungi, bacteria, viruses, mites and thrips is still the major problem that has hampered the establishment of truly aseptic plants and their successful Micro -propagation in bioreactors. The influence of bacteria on shoot growth can range from total inhibition to no apparent effect. The contaminating bacteria and fungi may be endophytic

or epiphytic, pathogenic or saprophytic (Debergh and Maene, 1981, 1984). Another type of hazard for plant tissue and cell cultures is caused by 'latent' bacteria and viruses that do not produce any symptoms on the plant or any visible growth on the medium for long periods of time in vitro even after several subculture cycles. They reduce the multiplication rates and productivity of tissue cultures and may become 'virulent' at a later stage due to changes in incubation temperatures, growth medium composition and removal of antibiotics from the medium (Leifert and Waites, 1998). Increasing attention is being paid to ascertain sources of contamination, to develop procedures for their elimination by avoidance, rigorous manipulation of the nutritional and environmental conditions and by specific antibiotic treatments (DeFossard and DeFossard, 1988; Debergh and Read, 1991).

3.4 Control of Contamination

Prevention of contamination in bioreactors requires a proper handling of the plant material, equipment and cultures during transfers and production. Only the surface sterilized explants, multiplied in small vessels and indexed for freedom from diseases are used to initiate cultures in bioreactors. If the bioreactor is small, it is sterilized in an autoclavable plastic bag, sealed with a cotton wool plug, and opened only under the laminar flow cabinet. If the bioreactor is large, other methods to protect the vessel after autoclaving and during its transport to the sterile area must be provided. The vessel is assembled under laminar flow, taking care that non-sterile objects do not enter the sterile air stream in the vicinity of open ports. After inoculation, all the ports and covers are sealed and the bioreactor is brought to the growth room and connected to an air supply. For harvesting, the bioreactor is returned to the sterile area, and the ports or covers are opened so that the air stream cannot carry contamination from the outside. Despite the precautions taken in initiating cultures, bioreactors can become contaminated from the environment or from latent microbes in the culture. The contamination can be controlled with one or a combination of anti-microbial compounds, acidification of the media, and micro-filtration of the medium (Schmidt et al., 2004). While most of the fungal and bacterial diseases are eliminated during surface sterilization and culture, viruses survive through successive multiplication if the mother plant is infected (Sessitsch et al., 2002). Acidification of the medium (pH 3) has been used to control contamination in the multiplication of banana and in media for other crops (Leifert and Waites, 1998).

4. Conclusion

Bioreactors provide more precise control of the plant growth gaseous exchange, illumination, medium agitation, temperature and pH than the conventional culture vessels. Bioreactor based propagation of plants can increase rate of multiplication, growth of cultures, reduce space, energy and labour requirements in commercial micropropagation. They can therefore, be attractive to developing countries with regards to new or expanding plant tissue culture facilities, in combination with a conventional laboratory. However, to be cost- effective, use of bioreactors requires indexed plant cultures, and attention to aseptic procedures during handling of plant materials. Hence, the integration of bioreactors into production systems should only be attempted by facilities with skilled and experienced expertise because such systems involve more risks, associated with inherently difficult problems of contamination in liquid systems.



Temporary immersion bioreactors (TIBs) has the potential to boost the Nigerian economy by scaling up the production process and at the same time fulfilling the aspirations of the huge populace especially as regards food security.

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